

16. Heat Pipes in Electronics Cooling (2)

16.1 Pulsating Heat Pipes

16.1.1 Introduction

Conventional heat pipe technology has been successfully applied in the last thirty years for the thermal management of a variety of applications like heat exchangers, economizers, space applications, and electronics cooling, to cite a few .

Although a plethora of designs of classical heat pipes are available, recent industry trends have frequently shown the limitations of these conventional designs. This has led to the evolution of novel concepts fitting the needs of present industry demands. A relatively new and emerging technology, Pulsating or Loop-type Heat Pipes (PHP), as proposed by Akachi, represent one such field of investigation. This range of devices is projected to meet all present and possibly future specific requirements of the electronics cooling industry, owing to favorable operational characteristics coupled with relatively cheaper costs.

Although grouped as a subclass of the overall family of heat pipes, the subtle complexity of internal thermo-fluidic transport phenomena is quite unique, justifying the need for a completely different research outlook. A comprehensive theory of operation and a reliable database or tools for the design of PHPs according to a given microelectronics-cooling requirement still remain unrealized.

Nevertheless, the prospects are too promising to be ignored.

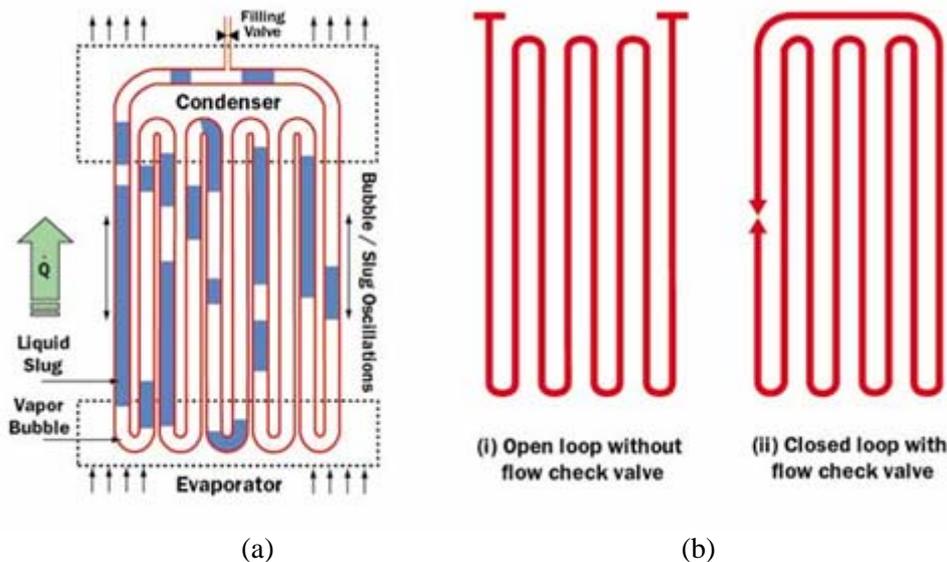


Figure 16.1:

- (a) Schematic of a closed loop pulsating heat pipe without check valve
 (b) Two types of possible layouts (i) Open loop (ii) Closed loop

16.1.2 Construction Details

A PHP consists of a plain meandering tube of capillary dimensions with many U-turns (Figure 16.1a). In contrast to a conventional heat pipe, there is no additional capillary structure inside the tube. There are two ways to arrange the tube: open loop and closed loop. As the names suggest, in a closed loop structure, the tube is joined end-to-end (Figure 16.1b). The tube is first evacuated and then filled partially with a working fluid, which distributes itself naturally in the form of liquid-vapor plugs and slugs inside the capillary tube. One end of this tube bundle receives heat, transferring it to the other end by a pulsating action of the liquid-vapor/bubble-slug system. There may exist an optional adiabatic zone

in between. Also, one or more flow-direction control check valves may be introduced at suitable locations to augment the performance. Figure 16.2 represents some practical design variations as proposed in.

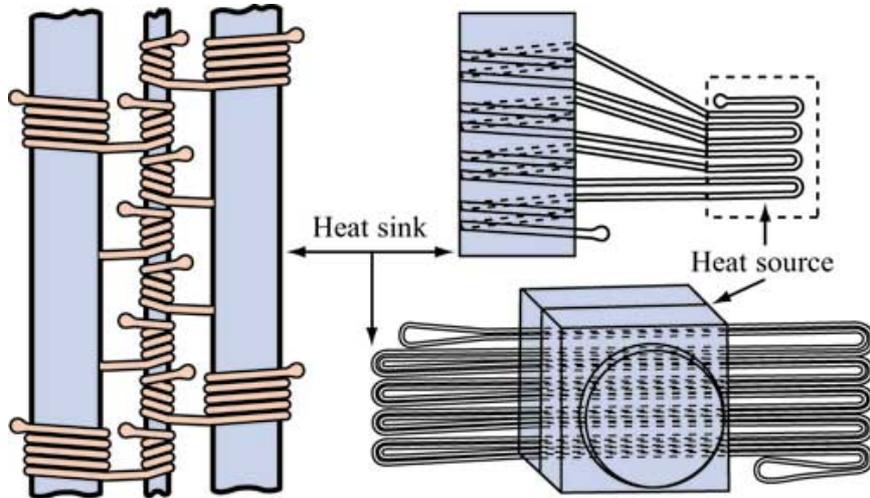


Figure 16.2: Some practical design variations of pulsating heat pipes.

16.1.3 Operational Features

A PHP is a complex heat transfer device with a strong thermo-hydraulic coupling governing its performance. It is essentially a non-equilibrium heat transfer device. The performance success of the device primarily depends on the continuous maintenance or sustenance of these non-equilibrium conditions within the system. The liquid and vapor slug transport results because of the pressure pulsations caused in the system. Since these pressure pulsations are fully thermally driven, because of the inherent constructions of the device, there is no external mechanical power source required for the fluid transport.

Consider a case when a PHP is kept isothermal throughout, say at room temperature. In this case, the liquid and vapor phases inside the device must exist in equilibrium at the saturated pressure corresponding to the fixed isothermal temperature. Referring to the pressure-enthalpy diagram, Figure 16.3, the thermodynamic state of all the liquid plugs, irrespective of their size and position, can be represented by point A. Similarly point B represents the thermodynamic state of all the vapor bubbles present in the PHP.

Suppose the temperature of the entire PHP structure is now quasi-statically increased to a new constant value. Then the system will again come to a new equilibrium temperature and corresponding saturation pressure, point A' and point B', in Figure 16.3. In doing so, there will be some evaporation mass transfer from the liquid until equilibrium is reached again. A similar phenomenon will be observed if the system is quasi-statically cooled to a new equilibrium condition A'' and B''.

In an actual working PHP, there exists a temperature gradient between the evaporator and the condenser section. Further, inherent perturbations are always present in real systems as a result of:

- Pressure fluctuations within the evaporator and condenser sections due to the local non uniform heat transfer always expected in real systems.
- Unsymmetrical liquid-vapor distributions causing uneven void fraction in the tubes.
- The presence of an approximately triangular or saw-tooth alternating component of pressure drop superimposed on the average pressure gradient in a capillary slug flow due to the presence of vapor bubbles.

The net effect of all these temperature gradients within the system is to cause non-equilibrium pressure condition which, as stated earlier, is the primary driving force for thermo-fluidic transport. As shown in

Figure 16.3, heating at the evaporator continuously tries to push point A upwards on the liquid saturation line of the pressure-enthalpy diagram. Simultaneously, point B is forced to move downwards on the vapor line at the other end.

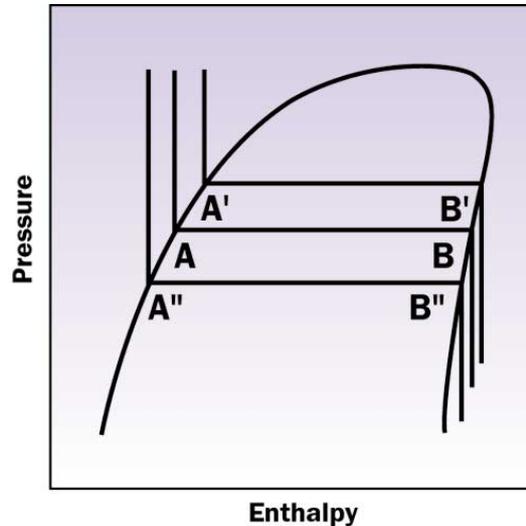


Figure 16.3: Typical pressure-enthalpy diagram

In this way a sustained non-equilibrium state exists between the driving thermal potentials and the natural causality, which tries to equalize the pressure in the system. Thus, a self-sustained thermally driven oscillating flow is obtained in a PHP. Note that no "classical steady state" occurs in PHP operation. Instead pressure waves and pulsations are generated in each of the individual tubes which interact with each other possibly generating secondary and ternary reflections with perturbations. From a force balance of gravity and surface tension leading to the definition of the Eötvös number, the theoretical maximum tolerable inner diameter (d_{crit}) of a PHP capillary tube can be calculated as:

$$d_{crit} = 2 \sqrt{\frac{\sigma}{g(\rho_{liq} - \rho_{vap})}} \quad \text{or} \quad \ddot{E}o = (Bo)^2 = 4$$

Where:

Bo	Bond number = $d \cdot (g(\rho_{liq} - \rho_{vap})/\sigma)^{0.5}$
D	Tube internal diameter (m)
Eö	Eötvös number = $(Bo)^2$
G	Acceleration due to gravity (m/s^2)
σ	Surface tension (N/m)
ρ	Liquid density (kg/m^3)

At diameters below this value, there is a tendency for surface tension forces to predominate, and this assists in formation of stable liquid slugs, an essential prerequisite for PHP operation. In vertical orientation, slug flow is known to exist even at bigger diameters in devices such as a standard bubble pump, depending on the heat flux. In horizontal flow, there exists a greater possibility of flow stratification as the diameter of the tube increases. In the light of these facts, the PHP critical diameter, as suggested above, requires further investigation to be established as a design rule.

13.1.4 Design Parameters

Various experimental investigations have been done with the aim of making a parametric study of a PHP. These studies indicate the following main variables affecting PHP performance:

- **Geometric Variables:** Overall length of the PHP, diameter/size and shape of the tube, length and number of turns of evaporator/condenser/adiabatic section.
- **Physical Variables:** Quantity of the working fluid (filling ratio), physical properties of the working fluid, tube material.

- **Operational Variables:** Open loop or closed loop operation, heating and cooling methodology, orientation of the PHP during operation, use of check valves.

It is evident that there are multiple variables which simultaneously affect the operation and performance of PHPs. Further, so far as capillary slug flow exists inside the entire device, it has been demonstrated that latent heat will not play a significant role in the device performance. Nevertheless, bubbles are certainly needed for self-sustained thermally driven oscillations.

On the other hand, under certain operating conditions, flow pattern transition to annular flow may occur. The probability of such an event is high with a combination of a high Eötvös number, high heat flux, and comparatively low liquid filling ratio ($\approx 50\%$ or lower). Note that if a flow regime changes from slug to annular, the respective roles of the latent and sensible heat transport mechanism may change considerably. This aspect requires further investigation.

So, the performance not only depends on a large number of parameters described above, but also on the flow pattern. This makes it all the more difficult to undertake mathematical modeling using conventional techniques.

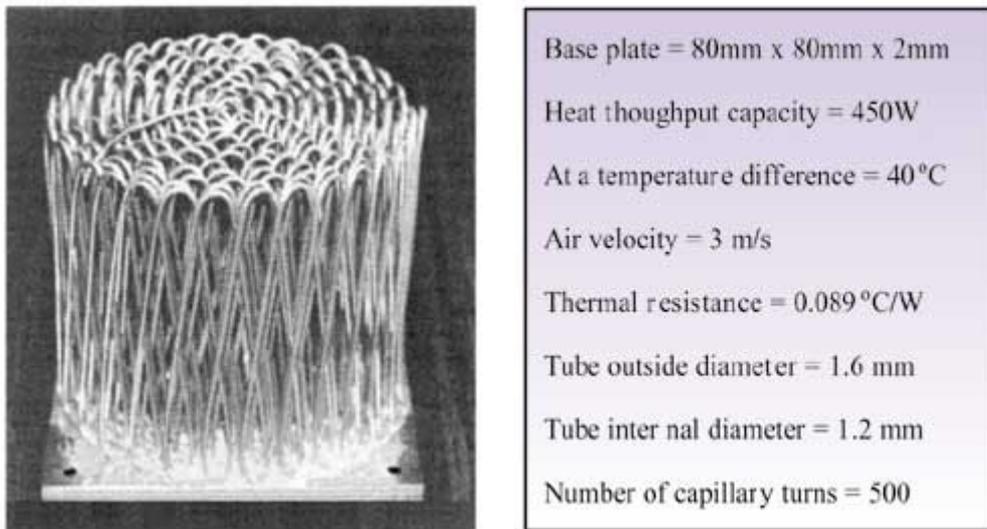


Figure 16. 4: A typical 'Kenzan Fin' and its performance data.

16.1.5 Typical Performance Data

Figure 16.4 shows a typical pulsating heat pipe, also referred to as "Kenzan Fin" which has been applied for cooling multi-chip modules. The thermal performance data is also included. The advantages of such systems can be summarized as follows:

- Compared to solid metal fins, this type of fin structure is certainly light weight.
- If optimal operation is achieved, this fin structure is thermally an order of magnitude better than equivalent solid fins even with an air cooling option.
- As the tube diameter is reduced, thermal performance of wicked conventional heat pipes is drastically reduced, while there is a parallel increase in manufacturing complexity and cost.

The latter fact is clear from Figure 16.5, which shows the maximum thermal performance of conventional wicked copper-water heat pipes of internal diameters 3 mm, 2.5 mm and 2.0 mm respectively in vertical orientation. In addition, PHPs have an edge over conventional wicked heat pipes as they are not limited by capillary or entrainment performance limits encountered in conventional heat pipes.

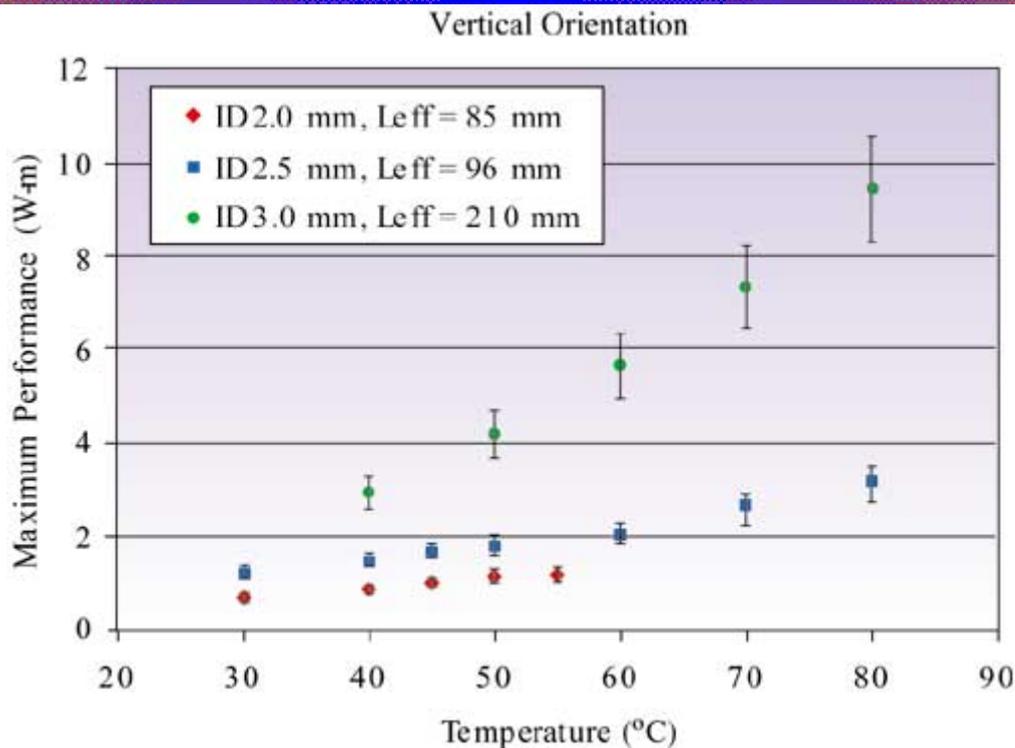


Figure 16.5: Maximum performance of miniature cylindrical copper-water conventional wicked heat pipes.

16.1.6 Conclusions

Pulsating Heat Pipes, apparently simple and very promising cooling devices, are very intriguing for theoretical and experimental investigations alike. They are attractive heat transfer elements, which due to their simple design, cost effectiveness, and excellent thermal performance may find wide applications. Since their invention in the early nineties, they have so far found market niches in electronics equipment cooling. Their complex operational behavior, which is not yet fully understood, has raised an ever growing academic interest. Until now, it has not been possible to simulate the PHP performances and there exists no complete engineering design tools.

16.2 Thermosyphons

16.2.1 Historical Development

The Thermosyphons was known as the Perkins tube was introduced by the Perkins family from the mid-nineteenth to the twentieth century through a series of patents in the United Kingdom. Most of the Perkins tubes were wickless gravity-assisted Thermosyphons, in which heat transfer was achieved by evaporation. The design of the Perkins tube, which is closest to the present heat pipe, was described in a patent by Jacob Perkins [1836]. A schematic drawing of the Perkins tube is shown in Figure 16.6 This design was a closed tube containing a small quantity of water operating in either a single- or two-phase cycle to transfer heat from a furnace to a boiler.

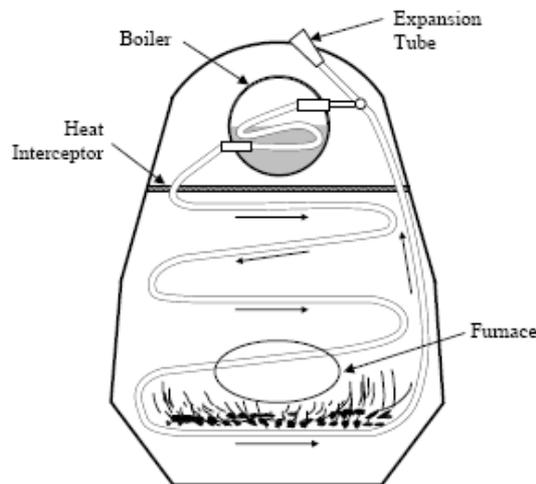


Figure 16.6: A schematic diagram of Perkins tube.

16.2.2 Principle of Operation

These are heat "transport" systems that use gravity to transfer heat (always gravity driven) from the source to sink or Thermosyphone refers to a heat transfer device in which the working fluid is circulated by the density difference between a cold temperature and a hot temperature fluid or between vapor and liquid, they can be put into a category of a cooling solution.

Thermosyphons transfer heat in exactly the same way as the Heat Pipe by evaporation followed by condensation. However no capillary structure is present to aid liquid transport from the condenser back to the evaporator, and thus the evaporator must be located vertically below the condenser, gravity will then ensure that the condensate returns to the evaporator.

To avoid the confusion because the term "Heat Pipe" is commonly used to describe both the Heat Pipe and Thermosyphone the term "Gravity Assisted Heat Pipe" has been used to describe Thermosyphons.

The features of the system can be summarized as follows:

- Requires no pump and reservoir/expansion tank, compared to closed loop cooling solutions.
- Can be made compact, so that the evaporator is the size of the module.
- Sensitive to orientation and internal fouling.
- Plumbed system, subject to shock/vibration, leakage, and potential dry-out

The most common industrial Thermosyphon applications include:

- Gas turbine blade cooling
- Electrical machine rotor cooling
- Transformer cooling
- Nuclear reactor cooling
- Steam tubes for baker's oven
- Cooling for internal combustion engines
- Electronic cooling.

16.2.3 Different Structure of Modern Thermosyphons

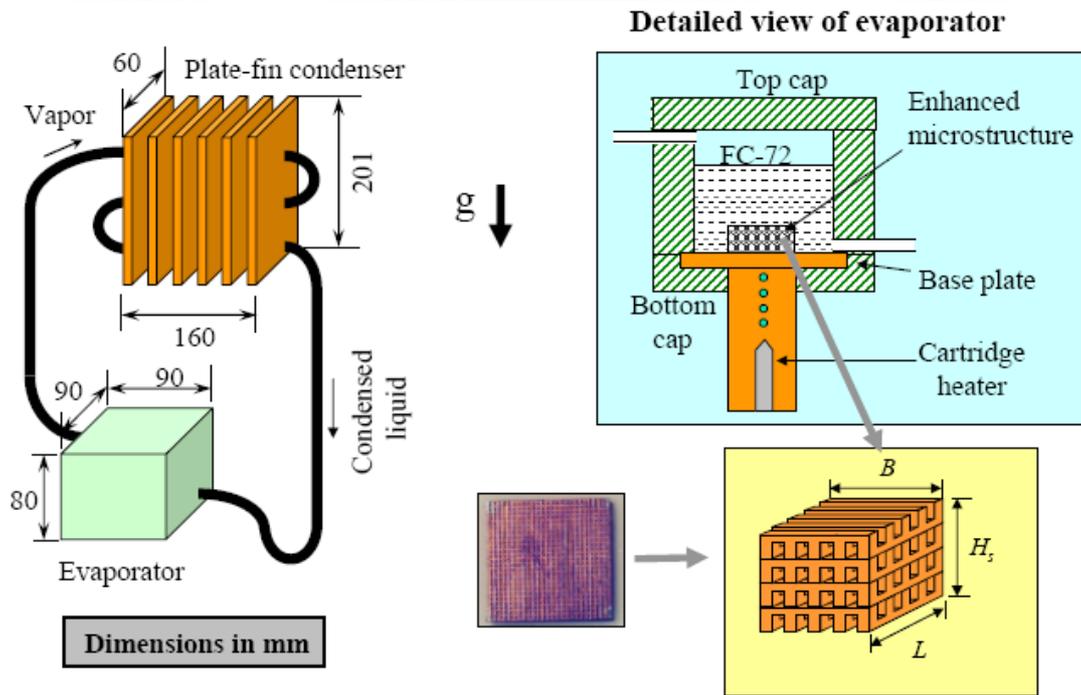


Figure 16.7: Thermosyphon incorporating enhanced structure.

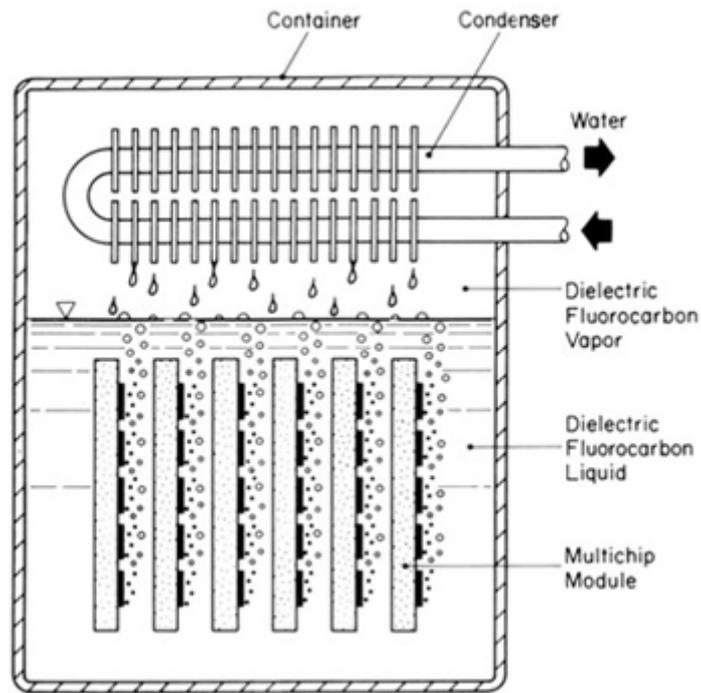
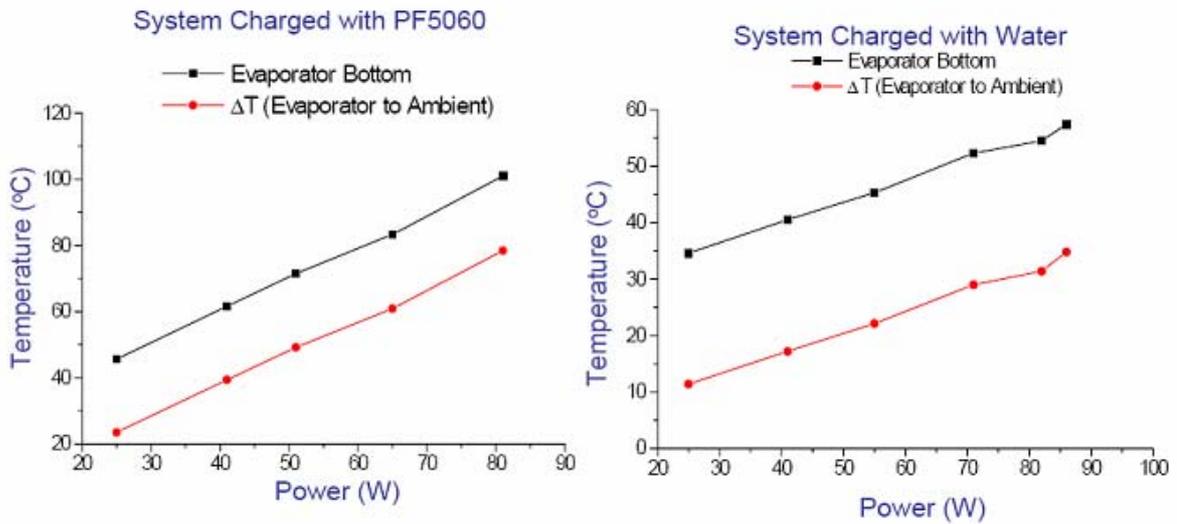
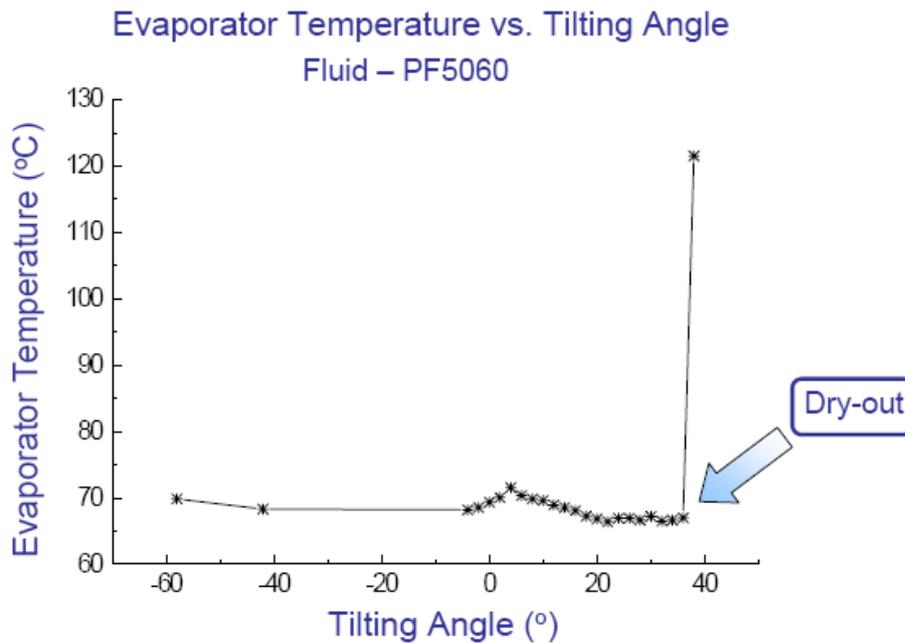


Figure 16.8: Water-Cooled multi chip module

16.2.4 Effect of Working Fluids



16.2.5 Effect of Inclination on the Thermosyphon



16.2.6 Comparison: Heat pipe and Thermosyphon

- Thermosyphon and heat pipe cooling both rely on evaporation and condensation. The difference between the two types is that in a heat pipe the liquid is returned from the condenser to the evaporator by surface tension acting in a wick, but Thermosyphon rely on gravity for the liquid return to the evaporator.
- However the cooling capacity of heat pipes is lower in general compared to the Thermosyphon with the same tube diameter.

16.2.7 Classification and Application of Thermosyphon System

- Open Thermosyphon
- Closed Thermosyphon
- Pipe Thermosyphon
 - Single-phase flow
 - Two-phase flow
- Simple loop Thermosyphon
 - Single-phase flow
 - Two-phase flow
- Closed advanced two-phase flow Thermosyphon loop